

Valve Concepts, Inc. ISO Registered Company


1" Model 1078
U.S. Pat. No. 4991620,5067522 and 5094267

## Application

On many low-pressure storage tanks the operating range is very low, which makes blanketing and venting system selection/design a challenge for the engineer. The Vacu-Gard ${ }^{\circledR}$ makes the job much easier. First, the Vacu-Gard ${ }^{\circledR}$ set point definition is where the blanketing valve closes bubble tight. This gives the largest dead band between the blanketing valve set point and the set point of the relieving device, and therefore will reduce losses. Second, the Vacu-Gard ${ }^{\circledR}$ has a wide range of available settings, from vacuum to 14 psig , that make proper selection easier.

# Model 1078 <br> Vacu-Gard ${ }^{\circledR}$ Tank Blanketing Valve 1" \& 2" (DN25 \& DN50) 

The Model 1078 is a pilot-operated valve, specifically designed to reduce blanketing gas losses on lowpressure storage tanks. It opens and closes automatically as required, to maintain a closely controlled blanket pressure. The simple design, increases reliability and lowers maintenance cost.

## FEATURES

Versatile: $\quad$ Single valve system offers wide variety of configurations to meet every blanketing application. Self cleaning flow design.

Top entry Compact and light weight yet Design:

Stability:

Performance: Valve set point can be verified $100 \%$ on the tank, without removal and without flowing supply gas into the tank. Temperature changes have no appreciable effect on set point

[^0]
## Sizes

1" (DN25) Body
2" (DN50) Body

## Connections

1" \& 2" FNPT (screwed)
1" 150\# integral RF flanges'
1" 300\# weldneck RF flange
2" 150\# \& 300\# RF weldneck flanges
DN25 (PN40), DN50 (PN16) \& DN50 (PN40)
weldneck flanges.
Special configurations are available on request:
Any combination of above.
Larger size reducing flanges.

## Outlet Configurations

Horizontal or Vertical
Valves with FNPT connections can be configured in the field. Valves with weldneck flange connec tions, configuration must be specified at time of order.

## Sensing Options

Remote sensing
Integral dip tube sensing (Vertical Outlet Only)

## Supply Pressures

Minimum: 20 psig (1.38 Bar)
Maximum: 200 psig (13.83 Bar)

| Pressure - Temperature Specifications |  |  |  |
| :---: | :---: | :---: | :---: |
| Body Material | End Connection | Inlet <br> Pressure | Temperature $\mathrm{F}(\mathrm{C})^{*}$ |
| Carbon <br> Steel ** | NPT, 150\# \& 300\#Flange | $\begin{gathered} 200 \text { psig } \\ \text { (13.8 Barg) } \end{gathered}$ | $\begin{gathered} -20 \text { to } 400 \\ (-29 \text { to } 204) \end{gathered}$ |
| Stainless Steel A351 CF3M | NPT \& 300\# <br> Flange | $\begin{gathered} 200 \mathrm{psig} \\ \text { (13.8 Barg) } \end{gathered}$ | $\begin{aligned} & -50 \text { to } 400 \\ & (-45 \text { to } 204) \end{aligned}$ |
|  | 150\# Flange | $\begin{gathered} 200 \\ (13.8 \text { Barg) } \end{gathered}$ | $\begin{gathered} \hline-325 \text { to } 300 \\ (-198 \text { to } 149) \end{gathered}$ |
|  |  | $\begin{gathered} 195 \\ \text { (13.4 Barg) } \end{gathered}$ | $\begin{gathered} \hline-325 \text { to } 400 \\ (-198 \text { to } 204) \\ \hline \end{gathered}$ |
| Hastelloy C ${ }^{\circledR}$ | NPT, 150\# \& 300\#Flange | $\begin{gathered} 200 \\ \text { (13.8 Barg) } \end{gathered}$ | $\begin{gathered} -50 \text { to } 400 \\ (-45 \text { to } 204) \end{gathered}$ |

* Design temperature limits maybe restricted by trim selection
** Only available in 2" (DN50) Size.
Hastelloy ${ }^{\circledR}$ is a registered trade name:
Hastelloy ${ }^{\text {® }}$ is a mark owned by Stelite Div., Cabot Corp.


## Capacities

See Table 6

## Outlet Pressure Ranges

See Table 3

## Maximum Back Pressures

25 psig (1.7 Bar)

## Materials of Construction

Diaphragm Case Material:
Carbon Steel (Powder Coated)
Stainless Steel
Hastelloy $\mathrm{C}^{\circledR}$
Trim Material:
316 Stainless Steel
Hastelloy $\mathrm{C}^{\text {® }}$
Diaphragm Material:
PTFE
Soft Seat \& Seals:
FKM is standard;
Buna-N, EPDM,
FFKM 1 - Similar to Chemraz
FFKM 2 - Similar to Kalrez

## Temperature Limits

Seat \& Seal Materials
FKM (Fluorocarbon Elastomer):
$-15^{\circ}$ to $300^{\circ} \mathrm{F}\left(-26^{\circ}\right.$ to $\left.149^{\circ} \mathrm{C}\right)$
Buna-N (Nitrile-NBR):
$-40^{\circ} \mathrm{F}$ to $212^{\circ} \mathrm{F}\left(-40^{\circ} \mathrm{C}\right.$ to $\left.100^{\circ} \mathrm{C}\right)$ EPDM (Ethylenepropylene):
$-55^{\circ} \mathrm{F}$ to $212^{\circ} \mathrm{F}\left(-48^{\circ} \mathrm{C}\right.$ to $\left.100^{\circ} \mathrm{C}\right)$
FFKM 1 (Perfluoroelastomer):
$-22^{\circ} \mathrm{F}$ to $400^{\circ} \mathrm{F}\left(-30^{\circ} \mathrm{C}\right.$ to $\left.204^{\circ} \mathrm{C}\right)$
FFKM 2 (Perfluoroelastomer):
$-40^{\circ} \mathrm{F}$ to $400^{\circ} \mathrm{F}\left(-40^{\circ} \mathrm{C}\right.$ to $\left.204^{\circ} \mathrm{C}\right)$

## Paint

Standard: Exterior coating will be a combination of Cashco Paint Specs \#S1777 epoxy and \#S-1743 powder coated. Tubing, fasteners, seat surfaces -corrosion resistant parts excluded.

## CAPACITY REQUIREMENTS

The capacity requirement of the tank blanketing valve is the sum of two components. The first being inbreathing due to liquid or product movement out of the tank and the second being inbreathing due to contraction of the vapors/product because of weather changes.

Inbreathing due to maximum liquid or product movement out of the tank equals 8.0 SCFH of air for each US gallon per minute of maximum emptying rate or $0.94 \mathrm{Nm}^{3} / \mathrm{h}$ of air for each $\mathrm{m}^{3} / \mathrm{h}$ of maximum emptying rate.

## Q displacement (SCFH) = Max. Pumpout Rate (gpm) x 8.0 <br> or

Q displacement $\left(\mathrm{Nm}^{3} / \mathrm{h}\right)=$ Max. Pumpout Rate $\left(\mathrm{m}^{3} / \mathrm{h}\right) \mathrm{X} .94$

The second component, inbreathing due to weather changes, is selected from Table 5 (Table $5 \mathrm{~A})$. The tank capacity is found in column 1 and the corresponding inbreathing requirement is selected from column 2.

The two components are added together to give the total inbreathing requirement and the capacity requirement of the tank blanketing valve.

$$
\mathbf{Q} \text { total = } \mathbf{Q} \text { displacement + } \mathbf{Q} \text { thermal }
$$

## VALVE SELECTION

If the tank blanketing supply pressure varies, use the minimum supply pressure in selecting the tank blanketing valve and the maximum supply pressure to determine blanketing valve failure capacity. Using the minimum supply pressure, select the size value from Table 6 that will meet the Total Inbreathing Requirement ( Q total). Next determine if a reducing "flow plug" can be used to make the capacity of the tank blanketing valve more closely match the inbreathing requirements. This will also reduce the fail open capacity of the blanketing valve. This is done by dividing the required inbreathing ( $Q$ total) by the full capacity of the size valve selected and multiplying by 100. Now from Table 2, choose the flow plug that is greater than the calculated percentage.

## Example:

Total inbreathing requirement $(Q$ total $)=25,850$ SCFH Maximum supply pressure $=100 \mathrm{psig}$ Minimum supply pressure $=80 \mathrm{psig}$

Next divide the total inbreathing requirement of 25,850 SCFH by the $1^{\prime \prime}$ valve capacity of 35,990 SCFH (at 80 psig) and multiply by 100 .
( 25,850 SCFH $/ 35,990$ SCFH $) \times 100=71.8 \%$
From Table 2, a $75 \%$ flow plug would be chosen for a 1 " valve. With the $75 \%$ flow plug, the blanketing valve will flow 26,993 SCFH at 80 psig and at the maximum supply pressure of 100 psig it will flow 32,693 SCFH. The 32,693 SCFH also represents the fail open flow of the blanketing valve and will be used in sizing the pressure relieving device.


## VALVE OPERATION

## Closed Position

Figure 1 shows the Vacu-Gard ${ }^{\circledR}$ in the closed position. This occurs when the tank pressure satisfies or exceeds the set pressure of the pilot. When the sensed pressure is sufficient to overcome the downward force of the set pressure spring, the pilot will close and there is no flow out of the pilot. This causes full supply pressure to accumulate in the chamber above the main valve piston. Since the piston area is larger than the seat area at the lower end of the piston, when the pressure above the piston is equal to the supply pressure the piston will move downward to close the valve due to the presence of a higher downward force.

## Open Position

Figure 2 shows the Vacu-Gard ${ }^{\text {® }}$ in the open position. When the tank pressure, that is sensed in the sense chamber below the diaphragm, is insufficient to hold against the downward force of the set pressure spring, the spindle in the pilot chamber will be forced downward. As the spindle unseats, the pressure in the pilot chamber will be discharged into the outlet of the valve. A small orifice restricts the gas flow into the pilot chamber from the supply pressure. Therefore, as soon as the pilot spindle opens, the pilot chamber pressure will drop significantly and will not be able to hold the main valve piston down. The piston will now be pushed full open by the supply pressure, allowing a maximum flow of the blanketing gas into the tank.

Once the tank pressure is back to set point, the spindle will close and the pilot pressure will rise to full supply pressure, pushing the main valve piston back down into the fully closed position.


Figure 1


Figure 2


The tank blanketing valve is not a substitute for the vacuum relief device.

API Standard 2000 states, "The design of a gas repressurizing system to eliminate the requirement for vacuum relief valves is beyond the scope of this standard and should be considered only when the induction of air represents a hazard equal to or greater than failure of the tank".

The tank blanketing valve failure must be taken into account when considering possible causes of overpressure in a tank.

API Standard 2000 states, "When the possible causes of overpressure or vacuum in a tank are being determined, other circumstances resulting from equipment failures and operating errors must be considered and evaluated by the designer." Failure of the tank blanketing valve can result in unrestricted gas flow into the tank, reduced gas flow or complete loss of the gas flow.

Tank blanketing valve set point definition is not the same for all manufacturers.

Valve Concepts defines set point as the point where the tank blanketing valve is closed bubble tight!

Some manufacturers define the set point as where the blanketing valve opens and the valve requires a pressure above the set point in order to close completely. Others define set point somewhere in between opening and closing but still the pressure must go above the defined set point in order to close completely.

The following example illustrates Valve Concepts Model 1078 definition of set point:


TABLE 5 REQUIREMENTS FOR THERMAL INBREATHING - ENGLISH UNITS (Air)

| REQUUREMENTS FOR THERMAL INBREATHING - ENGLISH UNITS (Air) |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| (Column 1) |  | (Column 2) | (Column 1) |  | (Column 2) |
| TANK CAPACITY |  | INBREATHING | TANK CAPACITY |  | GNBREATHING |
| Barrels | Gallons | SCFH | Barrels | Gallons | SCFH |
| 60 | 2,500 | 60 | 35,000 | $1,470,000$ | 31,000 |
| 100 | 4,200 | 100 | 40,000 | $1,680,000$ | 34,000 |
| 500 | 21,000 | 500 | 45,000 | $1,890,000$ | 37,000 |
| 1,000 | 42,000 | 1,000 | 50,000 | $2,100,000$ | 40,000 |
| 2,000 | 84,000 | 2,000 | 60,000 | $2,520,000$ | 44,000 |
| 3,000 | 126,000 | 3,000 | 70,000 | $2,940,000$ | 48,000 |
| 4,000 | 168,000 | 4,000 | 80,000 | $3,360,000$ | 52,000 |
| 5,000 | 210,000 | 5,000 | 90,000 | $3,780,000$ | 56,000 |
| 10,000 | 420,000 | 10,000 | 100,000 | $4,200,000$ | 60,000 |
| 15,000 | 630,000 | 15,000 | 120,000 | $5,040,000$ | 68,000 |
| 20,000 | 840,000 | 20,000 | 140,000 | $5,880,000$ | 75,000 |
| 25,000 | $1,050,000$ | 24,000 | 160,000 | $6,720,000$ | 82,000 |
| 30,000 | $1,260,000$ | 28,000 | 180,000 | $7,560,000$ | 90,000 |

NOTE: Table and sizing from API 2000 Seventh Edition, annex A, March 2014.

| TABLE 5A |  |  |  |
| :---: | :---: | :---: | :---: |
| REQUIREMENTS FOR THERMAL INBREATHING - METRIC UNITS (Air) |  |  |  |
| (Column 1) | (Column 2) | (Column 1) | (Column 2) |
| TANK CAPACITY | INBREATHING | TANK CAPACITY | INBREATHING |
| CUBIC METERS | Nm3/H | CUBIC METERS | Nm3/H |
| 10 | 1.69 | 5000 | 787 |
| 20 | 3.37 | 6000 | 896 |
| 100 | 16.9 | 7000 | 1003 |
| 200 | 33.7 | 8000 | 1077 |
| 300 | 50.6 | 9000 | 1136 |
| 500 | 84.3 | 10000 | 1210 |
| 700 | 118 | 12000 | 1345 |
| 1000 | 169 | 14000 | 1480 |
| 1500 | 253 | 16000 | 1615 |
| 2000 | 337 | 18000 | 1745 |
| 3000 | 506 | 20000 | 1877 |
| 3180 | 536 | 25000 | 2179 |
| 4000 | 647 | 30000 | 2495 |
| NOTE: Table and sizing from API 2000 Seventh Edition, annex A, March 2014. |  |  |  |


| TABLE 6 |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| TANK BLANKETING VALVE CAPACITIES |  |  |  |  |  |  |
| INLET PRESSURE psig (Barg) | CAPACITIES IN SCFH ( $\mathrm{Nm}^{3} / \mathrm{h}$ ) |  |  |  |  |  |
|  | AIR |  |  | NITROGEN |  |  |
|  | 1" Size | 1" HF Opt. | 2" Size | 1" Size | 1" HF Opt. | 2" Size |
| 20 (1.4) | 13,188 (353) | 22,279 (631) | 57,186 (1533) | 13,422 (359) | 22,671 (642) | 58,192 (1559) |
| 30 (2.1) | 16,990 (455) | 28,699 (813) | 73,666 (1974) | 17,290 (463) | 29,204 (827) | 74,962 (2009) |
| 40 (2.8) | 20,790 (557) | 35,119 (995) | 90,146 (2416) | 21158 (567) | 35,737 (1012) | 91,732 (2458) |
| 50 (3.4) | 24,590 (659) | 41,540 (1176) | 106,626 (2858) | 25,026 (670) | 42,271 (1197) | 108,502 (2907) |
| 60 (4.1) | 28,390 (761) | 47,960 (1358) | 123,106 (3299) | 28,894 (774) | 48,804 (1382) | 125,272 (3357) |
| 70 (4.8) | 32,190 (863) | 54,380 (1540) | 139,586 (3741) | 32,762 (878) | 55,337 (1567) | 142,042 (3806) |
| 80 (5.5) | 35,990 (965) | 60,801 (1722) | 156,066 (4183) | 36,630 (981) | 61,871 (1752) | 158,812 (4256) |
| 90 (6.2) | 39,790 (1066) | 67,221 (1904) | 172,546 (4624) | 40,498 (1085) | 68,404 (1937) | 175,582 (4705) |
| 100 (6.9) | 43,590 (1168) | 73,641 (2085) | 189,026 (5066) | 44,366 (1189) | 74,937 (2122) | 192,352 (5155) |
| 110 (7.6) | 47,390 (1270) | 80,062 (2267) | 205,506 (5508) | 48,234 (1292) | 81,470 (2307) | 209,122 (5604) |
| 120 (8.3) | 51,190 (1372) | 86,482 (2449) | 221,986 (5949) | 52,102 (1396) | 88,004 (2492) | 225,892 (6054) |
| 130 (9.0) | 54,990 (1474) | 92,902 (2631) | 238,466 (6391) | 55,970 (1499) | 94,537 (2677) | 242,662 (6503) |
| 140 (9.6) | 58,790 (1576) | 99,324 (2813) | 254,949 (6833) | 59,838 (1603) | 101,070 (2862) | 259,432 (6952) |
| 150 (10.3) | 62,590 (1677) | 105,743 (2995) | 271,426 (7274) | 63,706 (1707) | 107,604 (3047) | 276,202 (7402) |
| 160 (11.0) | 66,390 (1779) | 112,163 (3176) | 287,906 (7716) | 67,574 (1811) | 114,137 (3232) | 292,972 (7851) |
| 170 (11.7) | 70,190 (1881) | 118,584 (3358) | 304,386 (8158) | 71,442 (1914) | 120,670 (3417) | 309,742 (8301) |
| 180 (12.4) | 73,990 (1983) | 125,004 (3540) | 320,866 (8599) | 75,310 (2018) | 127,204 (3602) | 326,512 (8750) |
| 190 (13.1) | 77,790 (2085) | 131,424 (3722) | 337,346 (9041) | 79,178 (2122) | 133,737 (3787) | 343,282 (9200) |
| 200 (13.8) | 81,590 (2187) | 137,845 (3904) | 353,826 (9483) | 83,046 (2225) | 140,270 (3972) | 360,052 (9649) |

NOTE: To reduce flow capacity, use the flows plugs listed in Table 2. Reduced capacity will equal the flow plug percentage times the full flow capacity listed above.

1" Model 1078 DIMENSIONS

| RF FLANGES | A | B | C | D |
| :---: | :---: | :---: | :---: | :---: |
| $1^{\prime \prime}-150 \#$ Integral | $5.39^{\prime \prime}(136.9 \mathrm{~mm})$ | $3.07^{\prime \prime}(78.0 \mathrm{~mm})$ | $9.88^{\prime \prime}(250.9 \mathrm{~mm})$ | $3.69^{\prime \prime}(93.7 \mathrm{~mm})$ |
| $1^{\prime \prime}-300 \#$ Weldneck | $5.64^{\prime \prime}(143.3 \mathrm{~mm})$ | $3.32^{\prime \prime}(84.3 \mathrm{~mm})$ | $10.38^{\prime \prime}(263.6 \mathrm{~mm})$ | $3.94^{\prime \prime}(100.0 \mathrm{~mm})$ |



1" Model 1078 DIMENSIONS (cont.)


Hotizontal (Outlet), Integral 150\# RF Flange Body


Integral 150\# RF Flange Body with Tank and Pressure Gauges

## 1" Model 1078 DIMENSIONS (cont.)



Integral 150\# RF Flange Body with Purge Meter


Integral 150\# RF Flange Body with Gauges and Purge Meter

## 1" Model 1078 DIMENSIONS (cont.)



Highflow Option


| A | $9.5^{\prime \prime}(241 \mathrm{~mm})$ |
| :---: | ---: |
| B | $4.75^{\prime \prime}(121 \mathrm{~mm})$ |
| C | $5.5^{\prime \prime}(140 \mathrm{~mm})$ |
| D | $2.75^{\prime \prime}(70 \mathrm{~mm})$ |
| E | $6.67^{\prime \prime}(169 \mathrm{~mm})$ |
| F | $15.07^{\prime \prime}(383 \mathrm{~mm})$ |
| G | $2.5^{\prime \prime}(64 \mathrm{~mm})$ |



Vertical (Outlet), Weldneck RF Flange


| RF FLANGES | C | D |
| :---: | :---: | :---: |
| $2^{\prime \prime}-150 \#$ Weldneck | $14.69^{\prime \prime}(373.1 \mathrm{~mm})$ | $5.70^{\prime \prime}(144.8 \mathrm{~mm})$ |
| $2^{\prime \prime}-300 \#$ Weldneck | $15.19^{\prime \prime}(385.8 \mathrm{~mm})$ | $5.95^{\prime \prime}(151.1 \mathrm{~mm})$ |

## Horizontal (Outlet), Weldneck RF Flange

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## Supply Pressure Gauge

To provide local indication of supply pressure.

- Standard ABS gauge with SST fitting.
- Stainless gauge with SST fitting.


## Control Pressure Gauge

To provide local indication of actual tank pressure.

- Standard Magnehelic ${ }^{\circledR}$ gauge with SST fitting.
- Stainless gauge with SST fitting.


## Purge

A purge is used to prevent tank vapors from entering into the valve, specifically the pilot. One Variable Area Flow meter (Rotameter) is used to purge both the sense line and the outlet. The combined flow is $1-1.5 \mathrm{SCFH}$. VCI advises the use of a purge when tank vapors may solidify or crystallize when cooled to ambient temperature.

A purge will also extend the service life of the valve if 316 SST is not compatible with the tank vapors.

- Standard Rotameter used has a 316 SST body with glass tube.


## Sense with Dip Tube (patented) PV-Gard Manifold

The PV-Manifold allows for a very compact installation of a blanketing valve and vent valve on one single tank nozzle. Normally, an installation of this type requires at least three different nozzles; one for the blanketing valve, one for the vent valve, and one for the remote sensing for the blanketing valve. Using the PV-Manifold, only one tank nozzle is required.
Blanketing valves must be horizontal outlet with remote sensing.


This option provides a sense connection into the tank through the vertical outlet of the valve. This can be useful when no tank connection is available for the standard external sense.

- The dip tube length should be sized so that it protrudes 6 " to 8 " below the tank roof into the tank.
- The dip tube diameter is $0.3755^{\prime \prime}(9.52 \mathrm{~mm})$.
- Standard material is 316 SST.
- If orderd with 2049, Dip Tube cannot be offered.


NOTE: Customer must specify length of Dip Tube. Inline Filter

The valve comes standard with a pre-filter and a pilot filter in the pilot supply line. Therefore the use of an in-line filter is not required for regular blanketing gases. An in-line strainer or filter can be provided on request.

Option -40: NACE CONSTRUCTION. Internal wetted portions meet NACE standard MR0175, when exterior of the vent is not directly exposed to a sour gas environment, buried, insulated or otherwise denied direct atmospheric exposure. SST body and Trim-Buna-N or FKM Seat and Seal materials only. NPT or Flanged Connection. (Flanged version requires post-weld stress relieving by heat treating.) SST external Filter with or without purge meter.


| POSITION 6 - GAUGE OPTION |  |  |  |  |  |  |  | CODE |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| No Gauges |  |  |  |  |  |  |  | 0 |
| Supply | Supply <br> Gauge <br> ONLY | Supply Pressure Gauge plus Tank Gauge for Low Pressure Range |  |  |  |  |  |  |
| Pressure Range |  | $\begin{gathered} 0-5 " \mathrm{wc} \\ (0-15 \mathrm{mbar}) \end{gathered}$ | $\begin{gathered} 0-10 " \mathrm{wc} \\ (0-25 \mathrm{mbar}) \end{gathered}$ | $\begin{gathered} 0-15 \text { "wc } \\ (0-40 \mathrm{mbar}) \end{gathered}$ | $\begin{gathered} 0-1 \mathrm{psig} \\ (0-80 \mathrm{mbar}) \end{gathered}$ | $\begin{gathered} 0-5 \mathrm{psig} \\ (0-350 \mathrm{mbar}) \end{gathered}$ | $\begin{gathered} 0-15 \mathrm{psig} \\ (0-1.03 \mathrm{barg}) \end{gathered}$ | $\begin{gathered} 0-20 \mathrm{psig} \\ \text { (0-2 barg) } \end{gathered}$ |
|  | CODE | CODE | CODE | CODE | CODE | CODE | CODE | CODE |
| 0-100 (0-6.9) | 1 | A | D | G | K | N | S | W |
| 0-160 (0-11.0) | 2 | B | E | H | L | P | T | Y |
| 0-200 (0-13.8) | 3 | C | F | J | M | R | V | \# |
| NO Supply Gauge |  | 4 | 5 | 6 | 7 | 8 | 9 | Z |
| NOTE: Hastelloy Gauges are not available. |  |  |  |  |  |  |  |  |


| POSITION 7 - End Connections |  |  |
| :---: | :---: | :---: |
| End Connections (Flanges are Weldneck Design Unless Stated Otherwise) | 1" Body size (P1)only | 2" Body size (P2)only |
|  | CODE | CODE |
| FNPT Connection | T | T |
| 150\# RF Threaded Flgs w/ nipples | A | A |
| 300\# RF Threaded Flgs w/ nipples | B | - |
| 150\# RF Flgs ( 1 " body size has integral flanges) | D | D |
| 300\# RF Flgs | E | E |
| 1-1/2" 150\# RF Reducing Flgs | K | - |
| 1-1/2" 300 \# RF Reducing Flgs | J | - |
| 2" 150\# RF Reducing Figs | F | - |
| 2" 300\# RF Reducing Figs | G | - |
| FNPT Inlet w/1" 150\# RF Threaded Flange attached w/Nipple on Outlet | L | - |
| DN25 / PN40 Flgs | M | - |
| DN50 / PN16 Flgs | - | P |
| DN50 / PN40 Flgs | - | R |
| DN50 / PN40 Reducing Flgs | S | - |
| 1" Highflow 150\# Flg | N | - |


| POSITION 8 - FLOW PLUG SIZES |  |  |  |
| :---: | :---: | :---: | :---: |
| 1" Size | CODE | 2" Size | CODE |
| $10 \%$ | $\mathbf{1}$ | $20 \%$ | D |
| $25 \%$ | $\mathbf{2}$ | $40 \%$ | $\mathbf{4}$ |
| $50 \%$ | $\mathbf{5}$ | $60 \%$ | $\mathbf{6}$ |
| $75 \%$ | $\mathbf{7}$ | $80 \%$ | $\mathbf{8}$ |
| $100 \%$ | C | $100 \%$ | C |
| $170 \%$ * | H |  |  |
| *Select for 1" HF Option. |  |  |  |


| POSITION 9 - SEATS \& SEALS |  |
| :---: | :---: |
| Material | CODE |
| Buna-N * | B |
| FFKM 1 | C |
| EPDM | E |
| FFKM 2 | K |
| FKM (std) * | V |
| * Use with NACE Construction. |  |

BALANCE OF PRODUCT
CODE POSITIONS "10 \& 11" ON FOLLOWING PAGE.

| POSITION 10 - RANGE SPRINGS |  | POSITION 11 - EXTERNAL PILOT FILTER / OPTION |  |  |
| :---: | :---: | :---: | :---: | :---: |
| Spring Range | CODE | Description | Std. <br> Paint | $\begin{aligned} & \text { Opt- } \\ & 950 \mathrm{~S} \end{aligned}$ |
| 0.50" - 5.0" wc (1.24-12.4 mbar) ** | 3 |  |  |  |
| 5" - 14" wc (12.4-34.8 mbar) | 6 |  | CODE |  |
|  | 7 | SST Filter w/Purge | A | 6 |
|  |  | NACE Const. SST Filter w/Purge | F | 7 |
| $1-1.5 \mathrm{psig}$ (69-103 mbar) | 8 | Special Aluminum Filter (UCC/Dow) | B | - |
| $1.5-3 \mathrm{psig}$ (103-207 mbar) | 9 |  | c | . |
| 3-14 psig (0.2-0.96 bar) | K | Alum/Zinc Filter w/Check Valve |  |  |
|  |  | Alum/Zinc Filter w/Check Valve \& Purge | M | - |
| 0" - 1.5 " wc vac (0-3.7 mbar) * | A | SST Filter w/Check Valve | D | 8 |
| 1.5" - 6" wc vac (3.7-14.8 mbar) * | C | Opt-40 NACE Const. SST Filter w/Check Valve | 2 | 9 |
| * SST Tank gauge is not available for these ranges <br> ** $0.50^{\prime \prime}-0.70^{\prime \prime}$ w.c.(1.24-1.8 mbarg) not available in $2^{\prime \prime}$. See Table 4. |  | SST Filter w/Check Valve \& Purge | L | G |
|  |  | Opt-40 NACE Const. SST Filter w/Check Valve \& Purge | 3 | J |
|  |  | Alum/Zinc Filter w/Purge | P | - |
|  |  | SST Filter | S | T |
|  |  | NACE Const. SST Filter | E | U |
| information on $\mathbf{A}$ |  | Alum/Zinc Filter | w | - |
| ges 17 \& 18 on the | M. | Hastelloy Screen (Filter) | H | - |

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[^0]:    Lower
    Maintenance
    Costs:

    Uses standard o-rings for seat and seals.

